

BGR-017PCT/US

U.S. APPLICATION NO. (If known, see 37 CFR 1.5)

10/048129

TRANSMITTAL LETTER TO THE UNITED STATES  
DESIGNATED/ELECTED OFFICE (DO/EO/US)  
CONCERNING A FILING UNDER 35 U.S.C. 371INTERNATIONAL APPLICATION NO. INTERNATIONAL FILING DATE  
PCT/US 00/40401 18 July 2000 (18.07.00)PRIORITY DATE CLAIMED  
21 July 1999 (21.07.99)TITLE OF INVENTION  
Enhanced Crossflow Heat Transfer

APPLICANT(S) FOR DO/EO/US

Larsen, Thomas L. and Jayaswal, Umesh K.

Applicant herewith submits to the United States Designated/Elected Office (DO/EO/US) the following items and other information:

1.  This is a **FIRST** submission of items concerning a filing under 35 U.S.C. 371.
2.  This is a **SECOND** or **SUBSEQUENT** submission of items concerning a filing under 35 U.S.C. 371.
3.  This express request to begin national examination procedures (35 U.S.C. 371(f)) at any time rather than delay examination until the expiration of the applicable time limit set in 35 U.S.C. 371(b) and PCT Articles 22 and 39(1).
4.  A proper Demand for International Preliminary Examination was made by the 19th month from the earliest claimed priority date.
5.  A copy of the International Application as filed (35 U.S.C. 371(c)(2))
  - a.  is transmitted herewith (required only if not transmitted by the International Bureau).
  - b.  has been transmitted by the International Bureau.
  - c.  is not required, as the application was filed in the United States Receiving Office (RO/US).
6.  A translation of the International Application into English (35 U.S.C. 371(c)(2)).
7.  Amendments to the claims of the International Application under PCT Article 19 (35 U.S.C. 371(c)(3))
  - a.  are transmitted herewith (required only if not transmitted by the International Bureau).
  - b.  have been transmitted by the International Bureau.
  - c.  have not been made; however, the time limit for making such amendments has NOT expired.
  - d.  have not been made and will not be made.
8.  A translation of the amendments to the claims under PCT Article 19 (35 U.S.C. 371(c)(3)).
9.  An oath or declaration of the inventor(s) (35 U.S.C. 371(c)(4)). executed by Umesh K. Jayaswal
10.  A translation of the annexes to the International Preliminary Examination Report under PCT Article 36 (35 U.S.C. 371(c)(5)).

## Items 11. to 16. below concern document(s) or information included:

11.  An Information Disclosure Statement under 37 CFR 1.97 and 1.98.
12.  An assignment document for recording. A separate cover sheet in compliance with 37 CFR 3.28 and 3.31 is included.
13.  A **FIRST** preliminary amendment.
- A **SECOND** or **SUBSEQUENT** preliminary amendment.
14.  A substitute specification.
15.  A change of power of attorney and/or address letter.
16.  Other items or information: Information Disclosure Statement and reference copies

## CERTIFICATION UNDER 37 C.F.R. § 1.10\*

(Express Mail label number is mandatory.)

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I hereby certify that this paper and the documents referred to as being transmitted therewith are being deposited with the United States Postal Service on this date January 14, 2002 in an envelope as "Express Mail Post Office to Addressee" Mailing Label Number ET063376739US addressed to the: Assistant Commissioner for Patents, Washington, D.C. 20231 U.S. Patent and Trademark Office, P.O. Box 2327, Arlington, VA 22202.

Leslie R. Silverstein  
(type or print name of person mailing paper)

Leslie R. Silverstein  
Signature of person mailing paper

U.S. APPLICATION NO. (if known) 10/048129		INTERNATIONAL APPLICATION NO.	ATTORNEY'S DOCKET NUMBER																																																				
<p>17. <input checked="" type="checkbox"/> The following fees are submitted:</p> <p><b>BASIC NATIONAL FEE (37 CFR 1.492 (a) (1) - (5) ):</b></p> <p>Neither international preliminary examination fee (37 CFR 1.482) nor international search fee (37 CFR 1.445(a)(2)) paid to USPTO and International Search Report not prepared by the EPO or JPO ..... \$970.00</p> <p>International preliminary examination fee (37 CFR 1.482) not paid to USPTO but International Search Report prepared by the EPO or JPO ..... \$840.00</p> <p>International preliminary examination fee (37 CFR 1.482) not paid to USPTO but international search fee (37 CFR 1.445(a)(2)) paid to USPTO ..... \$690.00</p> <p>International preliminary examination fee paid to USPTO (37 CFR 1.482) but all claims did not satisfy provisions of PCT Article 33(1)-(4) ..... <del>\$710.00</del></p> <p>International preliminary examination fee paid to USPTO (37 CFR 1.482) and all claims satisfied provisions of PCT Article 33(1)-(4) ..... \$96.00</p>		<b>CALCULATIONS PTO USE ONLY</b>																																																					
<p><b>ENTER APPROPRIATE BASIC FEE AMOUNT =</b> \$ 710.00</p> <p>Surcharge of \$130.00 for furnishing the oath or declaration later than <input type="checkbox"/> 20 <input type="checkbox"/> 30 months from the earliest claimed priority date (37 CFR 1.492(e)). \$</p> <table border="1"> <tr> <td>CLAIMS</td> <td>NUMBER FILED</td> <td>NUMBER EXTRA</td> <td>RATE</td> </tr> <tr> <td>Total claims</td> <td>44 - 20 =</td> <td>24</td> <td>X \$18.00 \$432.00</td> </tr> <tr> <td>Independent claims</td> <td>2 - 3 =</td> <td>0</td> <td>X \$78.00 \$ 0</td> </tr> <tr> <td colspan="3"><b>MULTIPLE DEPENDENT CLAIM(S) (if applicable)</b></td> <td>+ \$260.00 \$</td> </tr> <tr> <td colspan="3"><b>TOTAL OF ABOVE CALCULATIONS</b></td> <td><b>\$ 1,142.00</b></td> </tr> <tr> <td colspan="3">Reduction of 1/2 for filing by small entity, if applicable. A Small Entity Statement must also be filed (Note 37 CFR 1.9, 1.27, 1.28).</td> <td>\$</td> </tr> <tr> <td colspan="3"><b>SUBTOTAL =</b></td> <td><b>\$ 1,142.00</b></td> </tr> <tr> <td colspan="3">Processing fee of \$130.00 for furnishing the English translation later than <input type="checkbox"/> 20 <input type="checkbox"/> 30 months from the earliest claimed priority date (37 CFR 1.492(f)). +</td> <td>\$</td> </tr> <tr> <td colspan="3"><b>TOTAL NATIONAL FEE =</b></td> <td><b>\$ 1,142.00</b></td> </tr> <tr> <td colspan="3">Fee for recording the enclosed assignment (37 CFR 1.21(h)). The assignment must be accompanied by an appropriate cover sheet (37 CFR 3.28, 3.31). \$40.00 per property +</td> <td>\$</td> </tr> <tr> <td colspan="3"><b>TOTAL FEES ENCLOSED =</b></td> <td><b>\$ 1,142.00</b></td> </tr> <tr> <td colspan="3"></td> <td><b>Amount to be refunded:</b> \$</td> </tr> <tr> <td colspan="3"></td> <td><b>charged:</b> \$</td> </tr> </table>				CLAIMS	NUMBER FILED	NUMBER EXTRA	RATE	Total claims	44 - 20 =	24	X \$18.00 \$432.00	Independent claims	2 - 3 =	0	X \$78.00 \$ 0	<b>MULTIPLE DEPENDENT CLAIM(S) (if applicable)</b>			+ \$260.00 \$	<b>TOTAL OF ABOVE CALCULATIONS</b>			<b>\$ 1,142.00</b>	Reduction of 1/2 for filing by small entity, if applicable. A Small Entity Statement must also be filed (Note 37 CFR 1.9, 1.27, 1.28).			\$	<b>SUBTOTAL =</b>			<b>\$ 1,142.00</b>	Processing fee of \$130.00 for furnishing the English translation later than <input type="checkbox"/> 20 <input type="checkbox"/> 30 months from the earliest claimed priority date (37 CFR 1.492(f)). +			\$	<b>TOTAL NATIONAL FEE =</b>			<b>\$ 1,142.00</b>	Fee for recording the enclosed assignment (37 CFR 1.21(h)). The assignment must be accompanied by an appropriate cover sheet (37 CFR 3.28, 3.31). \$40.00 per property +			\$	<b>TOTAL FEES ENCLOSED =</b>			<b>\$ 1,142.00</b>				<b>Amount to be refunded:</b> \$				<b>charged:</b> \$
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<p>a. <input checked="" type="checkbox"/> A check in the amount of \$ <u>1,142.00</u> to cover the above fees is enclosed.</p> <p>b. <input type="checkbox"/> Please charge my Deposit Account No. _____ in the amount of \$ _____ to cover the above fees. A duplicate copy of this sheet is enclosed.</p> <p>c. <input checked="" type="checkbox"/> The Commissioner is hereby authorized to charge any additional fees which may be required, or credit any overpayment to Deposit Account No. <u>50-1139</u>. A duplicate copy of this sheet is enclosed.</p>																																																							
<p><b>NOTE: Where an appropriate time limit under 37 CFR 1.494 or 1.495 has not been met, a petition to revive (37 CFR 1.137(a) or (b)) must be filed and granted to restore the application to pending status.</b></p>																																																							
SEND ALL CORRESPONDENCE TO		 SIGNATURE <u>David Silverstein</u> NAME																																																					
David Silverstein Andover-IP-Law 44 Park Street, Suite 300 Andover, MA 01810		<u>26,336</u> REGISTRATION NUMBER																																																					

10/048129  
531 Rec'd PCT/R 14 JAN 2002

Practitioner's Docket No. BGR-017PCT/US

CHAPTER II

#3/2

Preliminary Classification:

Proposed Class:

Subclass:

NOTE: "All applicants are requested to include a preliminary classification on newly filed patent applications. The preliminary classification, preferably class and subclass designations, should be identified in the upper right-hand corner of the letter of transmittal accompanying the application papers, for example 'Proposed Class 2, subclass 129.'" M.P.E.P., § 601, 7th ed.

**AMENDMENT ACCOMPANYING NEW APPLICATION TRANSMITTAL**

**(ENTRY INTO U.S. NATIONAL PHASE UNDER CHAPTER II)**

INTERNATIONAL APPLICATION NO.	INTERNATIONAL FILING DATE	PRIORITY DATE CLAIMED
PCT/US00/40401	18 July 2000 (18.07.00)	21 July 1999 (21.07.99)
<b>TITLE OF INVENTION</b>		
Enhanced Crossflow Heat Transfer		
<b>APPLICANT(S)</b>		
Washington Group International, Inc.; LARSEN, Thomas L.; JAYASWAL, Umesh K.		
<b>Box PCT</b>		
<b>Assistant Commissioner for Patents</b>		
Washington, D.C. 20231 U.S. Patent and Trademark Office		
ATTENTION: EO/US P.O. Box 2327		
Arlington, VA 22202		
Attention: EO/US		

**CERTIFICATION UNDER 37 C.F.R. § 1.10\***  
(Express Mail label number is mandatory.)  
(Express Mail certification is optional.)

I hereby certify that this Transmittal Letter and the papers indicated as being transmitted therewith is being deposited with the United States Postal Service on this date January 14, 2002, in an envelope as "Express Mail Post Office to Addressee" Mailing Label Number ET063376739US, addressed to the: Assistant Commissioner for Patents, ~~Washington, D.C. 20231~~ U.S. Patent and Trademark Office, P.O. Box 2327, Arlington, VA 22202

Leslie R. Silverstein

(type or print name of person mailing paper)

Leslie R. Silverstein

Signature of person mailing paper

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**\*WARNING:** Each paper or fee filed by "Express Mail" must have the number of the "Express Mail" mailing label placed thereon prior to mailing. 37 C.F.R. § 1.10(b).

"Since the filing of correspondence under § 1.10 without the Express Mail mailing label thereon is an oversight that can be avoided by the exercise of reasonable care, requests for waiver of this requirement will not be granted on petition." Notice of Oct. 24, 1996, 60 Fed. Reg. 56,430, at 56,442.

(Transmittal Letter to the United States Elected Office (EO/US) [13-18]—page 1 of 8)

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**PRELIMINARY AMENDMENT**

For the purposes of proceeding with this U.S. national stage application under 35 U.S.C. 371, please amend the claims of the above-identified PCT application as follows:

**In the Claims**

Cancel claims 1 – 38 without prejudice and substitute therefor new claims 39 – 82:

39. Fluid flow contouring apparatus for preferentially contouring the fluid path of a process fluid flowing cross-wise across and contacting a plurality of spaced-apart heat transfer conduits, said apparatus comprising a plurality of longitudinally continuous, sleeve-shaped baffle structures, each baffle structure comprising at least a paired set of fluid flow apertures which constitute the only upstream-to-downstream fluid passage through the fluid flow contouring apparatus, each of said baffle structures substantially symmetrically surrounding a heat transfer conduit to define an annular-shaped fluid flow region thereby isolating cross-wise fluid flow around that associated heat transfer conduit from cross-wise fluid flow around adjacent heat transfer conduits located transversely to the direction of fluid flow, and wherein the fluid flow apertures of a baffle structure are symmetrically located respectively upstream and downstream of the associated heat transfer conduit in at least partial upstream and downstream alignment with each other and with the associated heat transfer conduit, whereby each said baffle structure contours the flow path of said process fluid to establish a substantially uniform fluid flow pattern around the contour of the associated heat transfer conduit.

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40. Fluid flow contouring apparatus according to claim 39 wherein said heat transfer conduits comprise an array of cylindrical heat transfer conduits oriented to have parallel axes.

41. Fluid flow contouring apparatus according to claim 40 wherein each said baffle structure comprises a sleeve-shaped element which is substantially concentric relative to the associated heat transfer conduit.

42. Fluid flow contouring apparatus according to claim 41 wherein said paired sets of fluid flow apertures comprise upstream and downstream apertures in said sleeve-shaped elements.

43. Fluid flow contouring apparatus according to claim 39 wherein at least two of said baffle structures are interconnected into a larger flow contouring apparatus for contouring fluid flow around a plurality of heat transfer conduits.

44. Fluid flow contouring apparatus according to claim 40 wherein said heat transfer conduits are arranged in a generally circular array.

45. Fluid flow contouring apparatus according to claim 44 wherein the individual baffle structures associated with the heat transfer conduits are interconnected to form a larger, cylindrical-shaped flow contouring apparatus.

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46. Fluid flow contouring apparatus according to claim 45 wherein pairs of fluid flow apertures comprise radially-aligned upstream and downstream apertures in the individual baffle structures.

47. Fluid flow contouring apparatus according to claim 45 wherein pairs of fluid flow apertures comprise upstream and downstream apertures in the individual baffle structures which are offset from the radial line.

48. Fluid flow contouring apparatus according to claim 39 wherein said heat transfer conduits comprise at least one generally circular array of axially aligned cylindrical heat transfer conduits, at least some of which are substantially surrounded by a substantially concentric apertured sleeve-shaped structure having upstream and downstream aperture pairs in columns parallel to the axis of the associated conduit, further wherein a sleeve-shaped structure is secured by a plate member to an adjacent sleeve-shaped structure to form a larger cylindrical structure.

49. Fluid flow contouring apparatus according to claim 48 wherein the aperture pairs comprise elongated slots, each slot having a long axis generally parallel to the axes of the heat transfer conduits.

50. Fluid flow contouring apparatus according to claim 49 wherein pairs of elongated slots are in radial alignment.

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51. Fluid flow contouring apparatus according to claim 49 wherein a heat transfer conduit is associated with two pairs of elongated slots, each slot pair being offset from radial alignment with the axis of the larger cylindrical structure.

52. Fluid flow contouring apparatus according to claim 51 wherein the two upstream and the two downstream elongated slots associated with each heat transfer conduit are axially offset from one another but axially aligned with the opposite pair member.

53. Fluid flow contouring apparatus according to claim 48 wherein said heat transfer conduits comprise at least two generally circular arrays of cylindrical heat transfer conduits oriented to have parallel axes, one array being concentric relative to the other.

54. Fluid flow contouring apparatus according to claim 53 wherein the aperture pairs comprise elongated slots in radial alignment, each slot having a long axis generally parallel to the axes of the heat transfer conduits.

55. Fluid flow contouring apparatus according to claim 53 wherein the baffle structures of adjacent pairs of radially-aligned heat transfer conduits are interconnected such that an aperture between the baffle structures serves as the downstream fluid flow aperture for one of the conduits and the upstream fluid flow aperture for the other.

56. Fluid flow contouring apparatus according to claim 55 wherein the aperture pairs comprise elongated slots in radial alignment, each slot having a long axis generally parallel to the axes of the heat transfer conduits.

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57. Fluid flow contouring apparatus according to claim 39 wherein said heat transfer conduits comprise a substantially rectangular array comprising at least three axially aligned rows of cylindrical heat transfer conduits oriented to have parallel axes, and wherein the associated baffle structures comprise generally concentric sleeve-shaped elements having upstream and downstream aperture pairs.

58. Fluid flow contouring apparatus according to claim 39 wherein said heat transfer conduits comprise a substantially rectangular array comprising at least three rows of cylindrical heat transfer conduits, with alternate rows being axially offset from adjacent upstream and downstream rows, the heat transfer conduits oriented to have parallel axes, and wherein the associated baffle structures comprise generally concentric sleeve-shaped elements having upstream and downstream aperture pairs.

59. Fluid flow contouring apparatus according to claim 39 wherein the baffle structure associated with a heat transfer conduit comprises a set of substantially flat plate members positioned in pairs edgewise alongside two sides of a heat transfer surface in proximity to without touching the surface, the planes of said plate members being oriented generally orthogonal to the fluid path of the process fluid, so as to define generally annular-shaped fluid flow regions having upstream and downstream aperture pairs around said heat transfer conduits.

60. Fluid flow contouring apparatus according to claim 39 wherein the baffle structure associated with a heat transfer conduit comprises contoured plate members positioned in pairs alongside two sides of the heat transfer conduit in proximity to without

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touching the surface of the conduit, said plate members having a contour corresponding respectively to the two sides of the heat transfer conduit so as to define generally annular-shaped fluid flow regions having upstream and downstream openings around said heat transfer conduits, said plate members being joined to other plate members associated with adjacent heat transfer conduits.

61. A method for enhancing heat transfer to or from a fluid flowing cross-wise in contact with the outer surfaces of a plurality of heat exchange conduits comprising the step of preferentially contouring cross-wise fluid flow across the heat exchange conduits by flowing the fluid through at least a paired set of fluid flow constrictors in a longitudinally continuous, sleeve-shaped baffle structure associated with a heat exchange conduit, said baffle structure being part of an array of such baffle structures, each of which substantially symmetrically surrounds its associated heat exchange conduit to isolate cross-wise fluid flow around that associated heat exchange conduit from cross-wise fluid flow around adjacent heat exchange conduits located transversely to the direction of fluid flow, wherein the fluid flow constrictors of each baffle structure constitute the only upstream-to-downstream fluid passage through the baffle structure array and are symmetrically located respectively upstream and downstream of the associated heat exchange surface in at least partial upstream and downstream alignment with each other and with the associated heat exchange conduit, and whereby each baffle structure contours the flow path of said fluid to establish a substantially uniform fluid flow pattern around the contour of the associated heat exchange conduit.

62. A method according to claim 61 wherein said heat exchange conduits comprise an array of cylindrical heat exchange conduits oriented to have parallel axes.

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63. A method according to claim 62 wherein each said baffle structure comprises a sleeve-shaped element which is substantially concentric relative to the associated heat exchange conduit.

64. A method according to claim 63 wherein said paired sets of fluid flow constrictors comprise upstream and downstream apertures in said sleeve-shaped elements.

65. A method according to claim 61 wherein at least two of said baffle structures are interconnected into a larger flow contouring apparatus for contouring fluid flow around a plurality of heat exchange conduits.

66. A method according to claim 63 wherein said heat exchange conduits are arranged in a generally circular array.

67. A method according to claim 66 wherein the individual baffle structures associated with the heat exchange conduits are interconnected to form a larger, cylindrical-shaped flow contouring apparatus.

68. A method according to claim 67 wherein pairs of fluid flow constrictors comprise radially-aligned upstream and downstream apertures in the individual baffle structures.

69. A method according to claim 67 wherein pairs of fluid flow constrictors comprise upstream and downstream apertures in the individual baffle structures which are offset from the radial line.

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70. A method according to claim 61 wherein said heat exchange conduits comprise at least one generally circular array of axially aligned cylindrical heat exchange conduits, at least some of which are substantially surrounded by a substantially concentric apertured sleeve-shaped structure having upstream and downstream aperture pairs in columns parallel to the axis of the associated conduit, further wherein a sleeve-shaped structure is secured by a plate member to an adjacent sleeve-shaped structure to form a larger cylindrical structure.

71. A method according to claim 70 wherein the aperture pairs comprise elongated slots, each slot having a long axis generally parallel to the axes of the heat exchange conduits.

72. A method according to claim 71 wherein pairs of elongated slots are in radial alignment.

73. A method according to claim 71 wherein a heat exchange conduit is associated with two pairs of elongated slots, each slot pair being offset from radial alignment with the axis of the larger cylindrical structure.

74. A method according to claim 73 wherein the two upstream and the two downstream elongated slots associated with each heat exchange conduit are axially offset from one another but axially aligned with the opposite pair member.

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75. A method according to claim 70 wherein said heat exchange conduits comprise at least two generally circular arrays of cylindrical heat exchange conduits oriented to have parallel axes, one array being concentric relative to the other.

76. A method according to claim 75 wherein the aperture pairs comprise elongated slots in radial alignment, each slot having a long axis generally parallel to the axes of the heat exchange conduits.

77. A method according to claim 75 wherein the baffle structures of adjacent pairs of radially-aligned heat exchange conduits are interconnected such that an aperture between the baffle structures serves as the downstream fluid flow constrictor for one of the conduits and the upstream fluid flow constrictor for the other.

78. A method according to claim 77 wherein the aperture pairs comprise elongated slots in radial alignment, each slot having a long axis generally parallel to the axes of the heat exchange conduits.

79. A method according to claim 61 wherein said heat exchange conduits comprise a substantially rectangular array comprising at least three axially aligned rows of cylindrical heat exchange conduits oriented to have parallel axes, and wherein the associated baffle structures comprise generally concentric sleeve-shaped elements having upstream and downstream aperture pairs.

80. A method according to claim 62 wherein said heat exchange conduits comprise a substantially rectangular array comprising at least three rows of cylindrical heat

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exchange conduits, with alternate rows being axially offset from adjacent upstream and downstream rows, the heat exchange conduits oriented to have parallel axes, and wherein the associated baffle structures comprise generally concentric sleeve-shaped elements having upstream and downstream aperture pairs.

81. A method according to claim 61 wherein the baffle structure associated with a heat exchange conduit comprises a set of substantially flat plate members positioned in pairs edgewise alongside two sides of a heat exchange conduit in proximity to without touching the surface, the planes of said plate members being oriented generally orthogonal to the fluid path of the process fluid, so as to define generally annular-shaped fluid flow regions having upstream and downstream aperture pairs around said heat exchange conduits.

82. A method according to claim 61 wherein the baffle structure associated with a heat exchange conduit comprises contoured plate members positioned in pairs alongside two sides of the heat exchange conduit in proximity to without touching the surface, said plate members having a contour corresponding respectively to the two sides of the heat exchange conduit so as to define generally annular-shaped fluid flow regions having upstream and downstream openings around said heat exchange conduits, said plate members being joined to other plate members associated with adjacent heat exchange conduits.

### Remarks

In general, the purpose of this Preliminary Amendment is to amend the pending claims to better conform with amended claims 1 – 44 submitted by an Article 34 Amendment during Chap. II proceedings in the PCT application on which this Sec. 371 application is

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based. New claims 39 – 82 focus on the preferred embodiments of the present invention and better distinguish over the cited prior art.

Independent claims 39 (apparatus) and 61 (method) recite that each heat transfer/heat exchange conduit is substantially symmetrically surrounded by a longitudinally continuous, sleeve-shaped baffle structure having symmetrically positioned upstream and downstream apertures so as to isolate fluid flow around the associated heat transfer conduit from fluid flow around transversely adjacent heat transfer conduits in order to establish a substantially uniform fluid flow pattern around each heat transfer conduit.

Support for focusing on these preferred embodiments of the present invention, in which each heat transfer conduit has its own associated sleeve-like baffle structure to preferentially contour the cross-wise fluid flow path around that particular conduit, is found at page 7, line 21 to page 8, line 5 of the Specification. Additional support for the amended claims is found in the Summary of the Invention (pages 5 – 9) and in Figs. 2A, 3, 5, 6, 7 and 8 (as discussed in the Specification, each heat transfer conduit shown in the conduit arrays of Figs. 5 and 6 may include an associated apertured sleeve-like baffle structure – see Specification page 17, lines 2 – 3 and lines 18 – 19). As taught at page 8, lines 3 – 5 of the Specification: “Apertured sleeves of this type at least partially surrounding individual heat exchange conduits in an array of such conduits have been found to enhance heat transfer by a factor of about five times or more.”

The Written Opinion of August 13, 2001 during Chap. II proceedings in the corresponding PCT application cited the Ohsaki et al. (U.S. Pat. No. 4,594,227) and Dijt (U.S. Pat. No. 3,616,849) patents, specifically observing that “Dijt teaches cross-wise fluid flow paths for the purpose of increasing the heat transfer rate between the fluid and the

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tubes.” The Dijt patent further shows (Fig. 4) a type of baffle assembly for channeling fluid flow. The Ohsaki et al. ‘227 patent fails to show or suggest any type of baffle structure.

The present invention as herein claimed is distinguished from the Ohsaki et al. ‘227 and Dijt ‘849 patents in providing a very different, sleeve-shaped baffle system to substantially symmetrically surround each heat exchange conduit in an array of such conduits. The baffle system of the present invention differs from that shown in Dijt ‘849 in a number of important respects. First, Fig. 4 of Dijt does not show a baffle assembly which can be said to “substantially surround” any of the Dijt heat exchange conduits, as called for in independent claims 39 and 61. Second, Fig. 4 of Dijt does not provide a baffle assembly that comprises a lateral wall along each side of a heat exchange conduit. Therefore the Dijt design does not result in “isolating cross-wise fluid flow around that associated heat transfer conduit from cross-wise fluid flow around adjacent heat transfer conduits located transversely to the direction of fluid flow...” as called for in independent claims 39 and 61.

Third, the design in Fig. 4 of Dijt does not show “fluid flow apertures ... symmetrically located respectively upstream and downstream of the associated heat transfer conduit...” as recited in independent claims 39 and 61. Even assuming that the structure shown in Fig. 4 of Dijt could reasonably be interpreted as comprising both “upstream” and “downstream” flow constrictors, they are clearly not “symmetrically” located relative to a heat exchange conduit located between them because the “upstream” baffle element in Fig. 4 of Dijt ‘849 is clearly spaced farther from the conduit than is the “downstream” baffle element. This asymmetrical positioning results in a non-uniform fluid flow pattern around the conduit, as is clearly shown by the fluid flow arrows in Fig. 4 of Dijt. A fairer interpretation of Fig. 4 of Dijt would be to recognize that the Dijt structure provides only a

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downstream flow constrictor for each heat exchange conduit and does not provide an upstream flow constrictor in any meaningful sense of this term. Thus, there is no suggestion in either the Ohsaki et al. '227 patent or in the Dijt '849 patent of a fluid flow contouring apparatus and method as claimed herein.

The Sakuma et al. '919 patent cited in the accompanying Information Disclosure Statement recently came to Applicants' attention. Sakuma '919 is directed to a fin-and-tube heat exchanger somewhat similar in appearance and operation to an automobile radiator. A set of parallel fin plates (reference numeral 2 in Fig. 1 of Sakuma '919) channel fluid flow cross-wise across heat exchange tube 1, which is formed into a serpentine shape. Louvers 4, 5, 6 and 7 (Fig. 2 of Sakuma '919) are formed by slitting and bending these elements from the fin plates 2 such that they project alternately from opposite surfaces.

The stated objective of the Sakuma '919 patent is to improve heat transfer performance by minimizing the stagnant fluid zone which is conventionally generated behind (downstream) of the heat exchanger tube (see Fig. 24 - Prior Art of Sakuma '919). By contrast, in the heat exchanger according to the Sakuma '919 patent, "the rising ends of the louvers are slanted at an angle to the flow direction of the fluid which can smoothly direct the fluid flow behind the heat exchanger tube to prevent the fluid flow from detaching itself from the tube."

Although the louvers of Sakuma '919 clearly result in a certain type of contouring of fluid flow around the various sections of heat exchange tube 1, the structure, objective, and result of the Sakuma '919 design all differ dramatically from the present invention. More particularly, Sakuma '919 clearly does not teach or suggest the concept of substantially surrounding a heat exchange conduit with an apertured, sleeve-shaped, longitudinally

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continuous shell, as taught by the present invention, in order to isolate cross-wise fluid flow around each heat exchange conduit. In addition, louvers 4, 5, 6 and 7 projecting alternately from opposite fin plate surfaces do not provide a longitudinally continuous surface because these louvers are associated with separate fin plates and are not joined at the centerline between adjacent fin plates 2. The upstream louver configuration is not symmetrical with the downstream louver configuration (i.e., louvers 6 and 7 explicitly differ in shape from louver 5 to create an asymmetrical flow pattern), and the flat sides of the louvers do not conform to the curved shape of the heat exchange tube.

Another significant difference is that in the heat exchange design of Sakuma et al. '919, substantial portions of the cross-wise fluid flow can and do bypass one or even all of the multiple layers of heat exchange tubes, as seen for example in Fig. 5 and even more clearly in Fig. 17. Little if any of the fluid flow in Sakuma '919 ever directly contacts more than one section of heat exchange tube 1; and, as can be seen in Fig. 17, some portion of the fluid flow may never contact any part of tube 1. In Sakuma '919, however, some heat exchange appears to occur from fluid contacting fin plates 2 (which are connected to heat tube 1 by fin collars 3), even if that fluid bypasses direct contact with tube 1. Thus, preventing any fluid from bypassing the heat tube sections in Sakuma '919 would not be desirable and, in fact, would likely be impossible or render this system inoperable.

By contrast, the preferred sleeve-shaped baffle system of the present invention is expressly designed so as to prevent any fluid from bypassing any layer of heat exchange conduits (see, e.g., Figs. 2A and 3 of the present invention). Because all of the fluid flow in the present invention contacts every layer of heat exchange conduits, and because the fluid flow around each heat exchange conduit is preferentially contoured in accordance with this

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invention, the result is to produce a process stream that is heated/cooled both efficiently and with an extremely high degree of thermal uniformity. This makes such a process stream highly desirable for use in carrying out downstream chemical reactions where isolated "hot" spots or "cold" spots in a process feed could seriously degrade performance or product quality. The heat exchange system of Sakuma '919 is neither intended for nor able to achieve such a result.

**SUMMARY AND CONCLUSIONS**

For all of the foregoing reasons, claims 39 – 82 now pending should be deemed patentable.

Accordingly, this application is now considered to be in condition for allowance, and an early indication of same is earnestly solicited.

Respectfully submitted,

Date 1/14/02

  
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## ENHANCED CROSSFLOW HEAT TRANSFER

The present invention relates generally to methods and related apparatus for enhancing heat transfer to or from a fluid flowing cross-wise in contact with the outer thermally-conductive shells of a plurality of axially-oriented heat exchange conduits capable of acting as heat sources or heat sinks. By channeling cross-wise fluid flow, flowing generally orthogonal to the axes of the heat exchange conduits, and contouring it upstream, downstream and/or around or alongside the heat exchange conduits utilizing slotted or apertured plates, baffles or surrounding sleeve-like elements, a surprisingly more effective and efficient heat transfer between the flowing fluid and the thermally-conductive surface is realized.

### BACKGROUND OF THE INVENTION

It is well known to heat or cool process fluids, which may be liquids or gases, by flowing them into contact with a thermal-transfer surface that is maintained at a temperature which is different from that of the upstream process fluid thereby resulting in heat transfer either to or from the process fluid (depending on whether the thermal-transfer surface is maintained at a higher or lower temperature than the fluid). In one familiar version of this technology, the thermal-transfer surface that acts as a heat source or heat sink is the exterior of a thermally-conductive shell of a thermal-transfer tube or pipe, for example, which is heated or cooled by means of a liquid flowing axially through the interior of the tube or pipe. In a variation of this technology, heat may be supplied directly inside a heat exchange conduit by means of flameless combustion of fuel gas

(such as hydrogen or a hydrocarbon) as taught, for example, by U.S. Patent Nos. 5,255,742 and 5,404,952, which are incorporated herein by reference.

It is also known in the art to flow a process fluid axially along a thermal-transfer surface, either concurrently or counter-currently relative to the direction of liquid flow inside the thermal-transfer tube, or to crossflow the process fluid relative to the axis of the thermal-transfer tube, or some combination of the two. Typical applications of heat transfer between crossflowing fluid and heat exchanging conduits are found in air coolers, economizers associated with fired heaters or furnaces, and in shell and tube exchangers. Various types of so-called radial or axial/radial flow reactor designs are known for various applications whereby at least a part of a fluid process stream moves, at some point, through the reactor in a radial, crossflow direction (i.e., inward-to-out or outward-to-in), as contrasted with the more familiar axial flow (i.e., end-to-end) reactor designs. Examples of reactor designs embodying at least in part a radial, crossflow of process fluid relative to a plurality of axially-disposed heat-transfer tubes are shown in U.S. Patent Nos. 4,230,669; 4,321,234; 4,594,227; 4,714,592; 4,909,808; 5,250,270; and 5,585,074, each of which is incorporated herein by reference.

Although crossflow contact of a process fluid with a heat-transfer surface can be an attractive option for many applications, the utility of crossflow contact for industrial applications has been limited by certain heat transfer inefficiencies which have been experienced in practice. Typically in crossflow designs, a given portion of the process fluid is in contact with the heat-transfer surface for a shorter time than with a comparable axial flow design. In addition, the contact between the crossflowing process fluid and the

heat-transfer surface is uneven due to process fluid separation and recirculation. Short surface contact time, uneven contact, and limited fluid mixing can lead to inefficient, insufficient, and/or non-uniform thermal energy transfer.

Thus, in an article entitled "Impingement heat transfer at a circular cylinder due to an offset of non-offset slot jet," appearing in Int. J. Heat Mass Transfer., vol. 27, no. 12, pp. 2297-2306 (1984), the authors Sparrow and Alhomoud report experimental efforts to vary the heat transfer coefficients associated with crossflow of a process gas relative to a heat-transfer tube by positioning a slotted surface some distance upstream of the heat-transfer tube to create a gas jet. Sparrow and Alhomoud varied the width of the jet-inducing slot, the distance between the slot and the tube, the Reynolds number (degree of fluid turbulence), and whether the slot jet was aligned with or offset from the tube. The authors concluded that the heat transfer coefficient increased with slot width and Reynolds number, but decreased with slot-to-tube separation distance and offset.

Because the Sparrow and Alhomoud study concluded that the heat transfer coefficient increased with slot width, the general utility of an upstream slot to increase heat transfer is at best ambiguous based on these results. It can only be concluded that, in the experimental design used by Sparrow and Alhomoud, a relatively wider slot led to a higher heat transfer coefficient than a relatively narrower slot, and no upstream slot at all might yield the highest value. No testing was performed utilizing a plurality of heat-transfer tubes, or using upstream and downstream pairs, or around or alongside flow constriction means to preferentially contour crossflow fluid paths in contact with the outer surface of each of a plurality of heat-transfer tubes, and no reasonable extrapolations can

be made to such very different alternative designs and configurations based on the extremely limited data presented.

These and other drawbacks with and limitations of the prior art crossflow heat exchanged designs are overcome in whole or in part with the enhanced crossflow heat transfer methods and designs of this invention.

#### OBJECTS OF THE INVENTION

Accordingly, a principal object of this invention is to provide methods and designs for enhanced crossflow heat transfer between a process fluid and a heat-transfer surface.

It is a general object of this invention to provide methods and designs for specially directing and shaping fluid crossflow paths in contact with one or more heat-transfer surfaces so as to enhance heat transfer between the fluid and the heat-transfer surfaces.

A specific object of this invention is to provide fluid flow-constriction means upstream, downstream and/or around or alongside a heat-transfer surface so as to preferentially contour a process fluid stream flowing cross-wise past the heat-transfer surface to enhance heat transfer between the fluid stream and the heat-transfer surface.

A further specific object of this invention is to provide curved or flat apertured plates or apertured sleeves disposed relative to each conduit in an array of heat exchange

conduits so as to preferentially contour the flow path of the fluid stream flowing cross-wise past the outside of each of the conduits to realize improved heat transfer.

Still another object of this invention is to provide heat-transfer conduit arrays of varying sizes and configurations wherein each conduit of the array is associated with its own fluid flow-constriction means upstream, downstream and/or around or alongside of the conduit so as to preferentially contour the portion of the fluid stream flowing cross-wise past the outside of the conduit to realize improved heat transfer.

Other objects and advantages of the present invention will in part be obvious and will in part appear hereinafter. The invention accordingly comprises, but is not limited to, the methods and related apparatus, involving the several steps and the various components, and the relation and order of one or more such steps and components with respect to each of the others, as exemplified by the following description and the accompanying drawings. Various modifications of and variations on the method and apparatus as herein described will be apparent to those skilled in the art, and all such modifications and variations are considered within the scope of the invention.

#### SUMMARY OF THE INVENTION

In the present invention, a baffle structure comprising at least a paired set of fluid flow constructors is utilized to preferentially contour the flow path of a process fluid flowing cross-wise, or substantially cross-wise, in contact with a heat-transfer surface in order to enhance heat transfer between the fluid and the surface. The apparatus is

designed so as to substantially restrict the bypassing of fluid flow such that a predominant portion of the process fluid is forced to flow past the heat-transfer surface. The heat-transfer surface will typically be one or a configured array of heat exchange conduits, oriented to have parallel axes disposed in an axial direction which is generally orthogonal to the direction of fluid flow, and having a thermally-conductive shell. The exterior surface of the shell of each such conduit is maintained at a temperature different from that of the upstream process fluid so that thermal energy is transferred to or from the process fluid by means of conduction, convection, radiation or some combination thereof, as the fluid flows past and contacts the exterior surfaces of the heat exchange conduits.

The heat exchange conduits or ducts of this invention may broadly comprise tubes, pipes, or any other enclosures with heat sources or heat sinks. The exterior surfaces of the heat exchange conduits may be bare or, as discussed below, may be finned or any combination of the two. The cross-section of the conduits or ducts may be circular, elliptical, or any other closed shapes. Where a plurality of such heat exchange conduits are used, they will typically be arrayed in some predetermined configuration such as in a triangular array, a square array, a circular array, an annular array, or other such patterns depending on design choice and/or the requirements of a particular application. Relative to the direction of fluid flow, adjacent conduits may be aligned, staggered or otherwise positioned, again depending on design choice and/or application requirements.

The size of the heat exchange conduits will be dictated, at least in part, by process requirements for the rate of heat transfer. In general, conduits having larger cross-

sections (for any given conduit geometry) will provide larger surface areas and therefore more heat transfer capacity. Fin elements, baffles or other heat-transfer enhancing structures may be provided on the outside surface of some or all of the heat exchange conduits to further increase surface area and improve heat transfer characteristics. A preferred embodiment utilizes closely spaced circumferential fins applied in a spiral along the exterior length of the conduit. This arrangement increases the heat-transfer surface area exposed to the crossflow without impeding the flow. It will be understood that the nature and flowrate of the process fluid, and the desired temperature change in the fluid between upstream of the heat exchange conduits and downstream of the conduits, will also affect these design choices.

The fluid flow constriction means for contouring the cross-wise flow of the process fluid may comprise inlets, outlets and openings of various shapes and sizes in baffle structures located upstream, downstream and/or around or alongside the heat exchange conduits. In a further preferred embodiment, each heat exchange conduit has its own associated pair of upstream and downstream fluid flow constrictors or its own around or alongside flow constrictors as described below. The apertured baffle structures which function as fluid flow constriction means may comprise plates, sleeves or other baffles which comprise substantially flat surfaces, or curved surfaces, or a combination of flat and curved surfaces. Apertured structures of this type positioned in pairs upstream and downstream of an array of heat exchange conduits have been found to enhance heat transfer by a factor of about one and one-half to about two times. In a particularly advantageous embodiment for certain applications, the fluid flow constriction structure is a larger, generally concentric sleeve-like structure at least partially surrounding each

conduit in an array of tubular heat exchange conduits, each such sleeve structure having apertures upstream and downstream of the centrally-located heat exchange tube.

Apertured sleeves of this type at least partially surrounding individual heat exchange conduits in an array of such conduits have been found to enhance heat transfer by a factor of about five times or more.

The apertures in the fluid flow constriction structure preferably comprise any combination of perforated holes or axial slots (i.e., elongated apertures having a longer axis generally parallel to the axial orientation of the heat exchange conduits). The holes or slots in different portions of the apparatus may be the same or differ in curvature, size and shape. The edges around the inlets and outlets may be straight, rounded, jagged, or some combination thereof.

The fluid flow constriction structure is preferably positioned relative to an associated heat exchange conduit such that the distance between the centerline of an upstream or downstream aperture and the associated heat exchange conduit centroid ranges from about 0 to about 2.0, preferably from about 0.50 to about 1.00, times the outer diameter (or largest cross-sectional dimension of a non-circular conduit) of the conduit. In any case, the spacing between aperture and conduit must be sufficiently close to realize substantially enhanced heat transfer. The width (shortest side) of an elongated flow constriction aperture or the diameter of a generally circular hole constriction aperture may preferably range from about 0.02 to about 1.5, preferably from about 0.05 to about 0.25, times the outside diameter (or largest cross-sectional dimension of a non-circular conduit) of the conduit. The fluid flow constriction structure is preferably

positioned relative to an associated heat exchange conduit such that the offset between the center of the aperture and the centroid of the heat exchange conduit ranges from 0 to 0.5, preferably 0, times the outside diameter (or largest cross-sectional dimension of a non-circular conduit) of the conduit.

The enhanced crossflow heat exchange apparatus of this invention enhances heat transfer between the crossflowing fluid and the plurality of heat exchange conduits by one or more of the following mechanisms: (a) increasing the fluid velocity around the heat exchange conduits; (b) preferentially directing the fluid to closely follow the outer surface of the heat exchange conduits; (c) restricting the fluid from flowing into or through areas that are distant from the outer surface of a heat exchange conduit; (d) reducing "dead" regions and flow recirculation around heat exchange conduits; (e) enhancing fluid turbulence; and (f) enhancing mixing between colder and hotter portions of the fluid.

#### BRIEF DESCRIPTION OF THE DRAWINGS

Fig. 1 is a schematic top sectional view of a first embodiment of a crossflow heat exchange apparatus, with heat transfer enhancement according to the present invention, wherein a substantially circular array of axially-disposed heat exchange conduits is positioned inside a fluid flow-constricted annulus.

Fig. 2A is a schematic plan view of a second embodiment of a crossflow heat exchange apparatus, with heat transfer enhancement according to the present invention, showing a substantially circular array of axially-disposed heat exchange conduits, each

surrounded by a substantially concentric fluid flow-constricted tubular sleeve, and also showing the several fluid flow-constricted sleeves joined together in a first ring-like structure. Fig. 2B is a side view of one conduit-sleeve combination illustrating a preferred staggered offset slot configuration.

Fig. 3 illustrates a variation of the structure of Fig. 2 showing a double, concentric circular array of heat exchange conduits with radially adjacent conduits shown in alignment such that the fluid flow-restriction apertures of the respective flow-restricted sleeves associated with these radially aligned conduits are also in radial alignment.

Fig. 4 is a schematic top sectional view of another embodiment of a crossflow heat exchange apparatus, with heat transfer enhancement according to the present invention, showing a double row of axially-disposed heat exchange conduits arranged in a substantially rectangular array with a first, upstream fluid flow-restricted baffle, a second, intermediate fluid flow-restricted baffle separating the first and second rows of conduits, and a third, downstream fluid flow-restricted baffle following the second row of conduits, with the corresponding apertures of the first, second and third baffles shown substantially in alignment with the respective conduits and with each other.

Fig. 5 illustrates still another embodiment of an enhanced crossflow heat transfer apparatus according to this invention showing an array of multiple (i.e., three or more) rows of heat exchange conduits arranged in a triangular pitch and showing two alternative fluid flow paths through the array.

Fig. 6 illustrates another embodiment of an enhanced crossflow heat transfer apparatus according to this invention showing an array of multiple (i.e., three or more) rows of heat exchange conduits arranged in a square pitch and showing two alternative fluid flow paths through the array.

Fig. 7 illustrates still another embodiment of an enhanced crossflow heat transfer apparatus according to this invention showing how one or a plurality of plates can be positioned alongside two sides of each heat exchange conduit to cause preferential contouring of a crossflowing fluid stream to achieve enhanced heat transfer characteristics.

Fig. 8 illustrates yet another embodiment of an enhanced crossflow heat transfer apparatus according to this invention showing an alternative type of sleeve structure formed by positioning curved plates having a contour corresponding to two sides of a conduit around two sides of each heat exchange conduit to cause preferential contouring of a crossflowing fluid stream to achieve enhanced heat transfer characteristics.

#### DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENTS

Fig. 1 shows a crossflow heat exchange apparatus 10 according to this invention having a generally circular array of axially-disposed heat exchange conduits 12 distributed around the interior of an annular region 28 defined by an inner cylindrical wall 20 and an outer cylindrical wall 22, each having a common centerpoint 14. As shown in

Fig. 1, conduits 12 are of substantially the same diameter, which is less than the radial width of the annular region, and spaced substantially equidistant from one another.

Associated with each heat exchange conduit 12 is an upstream aperture 24 in inner wall 20 and a downstream aperture 26 in outer wall 22. As shown in Fig. 1, respective pairs of upstream apertures 24 and downstream apertures 26 are substantially in radial alignment with the associated conduit 12 and with each other. Thus, in Fig. 1, a process fluid 30 is flowed axially into the inner cylindrical region 16 of the heat exchange apparatus 10 and then directed radially outward through upstream apertures 24, flowing cross-wise into contact with the heat exchange conduits 12, as denoted by the fluid flow arrows in Fig. 1, thereby heating or cooling the process stream to form a thermally-conditioned fluid stream 32 which exits annular region 28 through downstream apertures 26.

It will be understood that whereas Fig. 1 illustrates a radially-outward fluid flow path, the same apparatus could be utilized for thermally treating a process stream flowing radially inward to center region 16 and thereafter being axially withdrawn from region 16. In this variation, apertures 26 in the outer wall 22 would be the upstream apertures and apertures 24 in inner wall 20 would be the downstream apertures.

Figs. 2A and 2B show a particularly preferred crossflow heat exchange apparatus 110 according to this invention having a generally circular array of axially-disposed heat exchange conduits 112, each surrounded by an apertured sleeve 120 having either an upstream aperture 124 and a downstream aperture 126 or offset aperture pairs 174, 176

and 184, 186 as described below. The individual sleeves 120 are joined together into a larger ring-like or cylindrical structure by connecting walls 122. Apertures 124 and 126 may comprise columns of axially-oriented perforation holes or elongated slots which are radially aligned with the conduits 112. Alternatively, in a preferred embodiment also illustrated in one portion of Fig. 2A, aperture pairs 174, 176 and 184, 186 are slightly offset from radial alignment in a staggered slot arrangement. The staggered slot arrangement for aperture pairs 174, 176 and 184, 186 is illustrated in Fig. 2A, with additional detail in Fig. 2B, where offset slot pairs 174, 176 and 184, 186 (replacing apertures pairs 124, 126) are staggered in elevation and offset slightly from the radial line from centerpoint 114 by equal angles  $\theta$ . Fig. 2B shows a side view taken along the line 2B-2B in Fig. 2A of a heat exchange conduit 112 having a cylindrical sleeve 120 with the preferred staggered slot arrangement. The plan view of this staggered slot conduit/sleeve combination as shown in Fig. 2A is taken along the line 2A-2A in Fig. 2B. The ends of the slots from alternating offset slot pairs can be slightly overlapped or at equal elevation so there is no interruption of flow along the axial direction of the heat exchange apparatus. This design with separation and overlap of the offset slots also leaves connection regions between the axially overlapped portions of adjacent offset slots, indicated generally by the reference numeral 190 in Fig. 2B, to provide the sleeves 120 with better circumferential mechanical integrity without blocking any fluid flow. For simplified illustration, Fig. 2A shows one apertured sleeve 120 having the two-pair offset aperture configuration while the other sleeves have the one-pair aligned aperture configuration. In practice, however, all of the apertured sleeves for a particular apparatus 110 will typically have the same aperture configuration.

Thus, in Fig. 2A, a process fluid 130 is flowed axially into the inner cylindrical region 116 having centerpoint 114 of the heat exchange apparatus 110 and then directed radially outward through upstream apertures 124, flowing cross-wise into contact with the heat exchange conduits 112, as denoted by the fluid flow arrows in Fig. 2A, thereby heating or cooling the process stream to form a thermally-conditioned fluid stream 132 which exits the interior regions defined by the sleeves 120 through downstream apertures 126. In the staggered slot embodiment, fluid flowing radially outward would either flow through upstream aperture 174, into contact with conduit 112, and exit through downstream aperture 176, or, depending on the axial elevation, instead flow through aperture pair 184, 186. It will be understood that whereas Fig. 2A illustrates a radially-outward fluid flow path, the same apparatus could be utilized for thermally treating a process stream flowing radially inward to center region 116 and thereafter being axially withdrawn from region 116. In this variation, apertures 126 (or 176 and 186) would be the upstream apertures, and apertures 124 (or 174 and 184) would be the downstream apertures.

Fig. 3 shows a crossflow heat exchange apparatus 160 which is a variation of the crossflow heat exchange apparatus 110 shown in Fig. 2. Apparatus 160 differs from apparatus 110 in the use of a double, concentric circular array of heat exchange conduits instead of the single circular array of Fig. 2. As seen in Fig. 3, there is a second circular array of heat exchange conduits 142, each in radial alignment with a corresponding conduit 112 of the first circular array. Each conduit 142 is surrounded by an apertured sleeve 150 having an upstream aperture 164 and a downstream aperture 166. Apertures 164 and 166 for a given sleeve 150 associated with a particular conduit 142 are shown

substantially in radial alignment with the apertures 124 and 126 in the sleeve 120 of the corresponding radially adjacent conduit 112. The individual sleeves 150 are joined together into a larger ring-like or cylindrical structure by walls 152. Although Fig. 3 shows only a single conduit 142 of the second circular array of heat exchange conduits, it will be understood that each conduit 112 of the first circular array is associated with a corresponding conduit 142 of the second circular array.

Thus, in Fig. 3, a partially thermally-conditioned fluid stream 132 exiting first downstream apertures 126 in sleeves 120 is directed radially outward through second upstream apertures 164, flowing cross-wise into contact with the second array of heat exchange conduits 142, thereby further heating or cooling the process stream to form a fully thermally-conditioned fluid stream 162 which exits the interior region defined by the sleeves 150 through second downstream apertures 166. It will be understood that whereas Fig. 3 illustrates a radially-outward fluid flow path, the same apparatus could be utilized for thermally treating a process stream flowing radially inward to center region 116 and thereafter being axially withdrawn from region 116. In this variation, apertures 166 and 126 would be respectively the first and second upstream apertures, and apertures 164 and 124 would be respectively the first and second downstream apertures.

Fig. 4 shows a portion of another crossflow heat exchange apparatus 210 according to this invention. In Fig. 4 a double row of axially-disposed heat exchange conduits, comprising a first upstream row of conduits 212 and second downstream row of conduits 216, are disposed in a generally rectangular array in conjunction with: a first, upstream apertured plate 220 having apertures 226; a second, intermediate apertured plate

222 having apertures 228, plate 222 separating the first and second rows of conduits; and, a third, downstream apertured plate 224 having apertures 230. Each set of apertures 226, 228 and 230 associated with an upstream-downstream adjacent pair of conduits 212 and 216 is shown substantially in linear alignment with each other and with the associated pair of upstream and downstream conduits 212 and 216 respectively.

Thus, in Fig. 4, a process fluid 232 is directed, as denoted by the fluid flow arrows in Fig. 4, through apertures 226 and flowed cross-wise into contact with first, upstream heat exchange conduits 212, thereby partially heating or cooling the process stream to form a partially thermally-conditioned fluid stream 234. Stream 234 is then directed through apertures 228 and flowed cross-wise into contact with second, downstream heat exchange conduits 216 thereby further heating or cooling the process stream to form a fully thermally-conditioned fluid stream 236 which is flowed out of the apparatus 210 through exit apertures 230.

Fig. 5 illustrates two alternative possible fluid flow paths through a multi-row set of heat exchange conduits 312 arranged in an offset or triangular array in accordance with another embodiment of a crossflow heat exchange apparatus 310 according to this invention. Thus, in Fig. 5, alternate rows of heat exchange conduits are offset from adjacent rows instead of having conduits in adjacent rows substantially in linear alignment as shown in Figs. 4 and 6. In this configuration, the centerpoints of three adjacent conduits in two adjacent rows form an equilateral triangle 340. Although not shown in Fig. 5, it is understood that the apparatus of Fig. 5 includes upstream and downstream apertured plates respectively located before the first row of conduits and

after the last row of conduits, as well as intermediate apertured plates separating adjacent rows of conduits. Alternatively, each conduit 312 may be surrounded with an apertured sleeve-like structure as previously described for other figures.

Fluid flow arrows 332 in Fig. 5 illustrate a first possible fluid flow orientation which can be utilized with the triangular conduit array of apparatus 310. Fluid flow arrows 334 in Fig. 5 illustrate a second possible fluid flow orientation which can be utilized with the triangular conduit array of apparatus 310. Although Fig. 5 shows four rows of heat exchange conduits in the triangular array, a smaller or larger number of conduit rows in this configuration may be utilized as appropriate.

Fig. 6 illustrates two alternative possible fluid flow paths through a multi-row set of heat exchange conduits 412 arranged in a square array in accordance with still another embodiment of a crossflow heat exchange apparatus 410 according to this invention. Thus, in Fig. 6, conduits 412 in adjacent rows are substantially in linear alignment. In this configuration, the centerpoint of four adjacent conduits in two adjacent rows form a square 440. Although not shown in Fig. 6, it is understood that the apparatus of Fig. 6 includes upstream and downstream apertured plates respectively located before the first row of conduits and after the last row of conduits, as well as intermediate apertured plates separating adjacent rows of conduits. Alternatively, each conduit 412 may be surrounded with an apertured sleeve as previously described.

Fluid flow arrows 432 in Fig. 6 illustrate a first possible fluid flow orientation which can be utilized with the square conduit array of apparatus 410. Fluid flow arrows

434 in Fig. 6 illustrate a second possible fluid flow orientation which can be utilized with the square conduit array of apparatus 410. Although Fig. 6 shows five rows of heat exchange conduits in the square array, a smaller or larger number of conduit rows in this configuration may be utilized as appropriate.

Fig. 7 illustrates still another variation of an enhanced crossflow heat transfer apparatus 510 according to this invention. In Fig. 7, each heat exchange conduit 512 is associated with one or more lateral flow-constriction plates 520, 522, 524, 526, and 528 positioned alongside conduit 512 and oriented generally orthogonal to the direction of fluid flow, as indicated by arrows 530 and 532. The edges of the lateral plates 520, 522, 524, 526 and 528 closest to conduit 512 are spaced apart from the exterior walls of conduit 512 so as to create two fluid openings or channels between the plate edges and the conduit wall, one along each side of each conduit 512. The spacing between the plate edges and the conduit wall may be adjusted by routine experimentation to optimize the contouring of the fluid flow path to maximize heat transfer. Where two or more lateral flow-constriction plates are utilized for each conduit 512, the spacing between the plate edges and the conduit wall may be the same or different in order to optimally contour the fluid flow path.

As seen in Fig. 7, the lateral flow-constriction plates may be positioned alongside conduit 512 such that the plane of the plate passes through the centroid 518 of conduit 512 (such as plate 524), or else be positioned such that the planes of the plates intersect conduit 512 upstream (such as plates 520 and 526) of centroid 518, or downstream (such as plates 522 and 528) of centroid 518, or any combination thereof. The distance 542

between the aperture and the conduit centroid 518 may be less than one-half of the diameter 544 as shown, with a distance approaching zero as a limit, for example plate 524. This differs from the baffle structures shown in Figs. 1 and 4 where the distance between the apertures and the conduit centroid is greater than one-half the diameter of the conduit. As used herein, the phrase "lateral plate positioned alongside a heat exchange conduit" is meant to refer to plates such as 520, 522, 524, 526 and 528 in Fig. 7, oriented generally orthogonal to the direction of fluid flow, wherein the plane of the plate intersects any part of the heat exchange conduit.

Fig. 8 illustrates another variation of an enhanced crossflow heat transfer apparatus 610 according to this invention showing a variation of the apertured sleeve configuration shown in Fig. 2. In Fig. 8, each heat exchange conduit 612 is partially surrounded by a pair of oppositely curved plates 620 generally conforming to the curvature of the outer wall of conduit 612 in a clam-shell configuration. Each curved plate 620 is joined to a wall or lateral plate 622 positioned generally orthogonal to the direction of fluid flow, as indicated by arrows 630 and 632.

The pair of curved plates 620 around either side of a given conduit 612 do not touch each other and do not extend either upstream or downstream of the outer wall of conduit 612. Thus, as shown for illustration purposes in Fig. 8, a line or plane connecting the upstream or downstream edges of a pair of curved plates 620 would intersect conduit 612. The upstream and downstream openings between the pairs of curved plates 620 are the apertures through which the process fluid stream is directed to realize preferential contouring of the fluid stream. The distance 642 between the aperture and the conduit

centroid 618 may be less than one-half of the diameter 644 as shown, with a distance approaching zero as a limit, for example, as the lengths of curved plates 620 approach zero leaving only lateral plate 622, a configuration corresponding to Fig. 7 with a single plate 524. This differs from the baffle structures shown in Figs. 1 and 4 where the distance between the apertures and the conduit centroid is greater than one-half the diameter of the conduit.

The clam-shell configuration of Fig. 8 with each pair of curved plates 620 around the sides of each conduit 612, differs from the slotted sleeve configuration of Fig. 2 in that in Fig. 8 a line or plane connecting the edges of the upstream and downstream fluid openings intersects the conduit 612, which is not the case for the slotted sleeves shown in Fig. 2A. In a sense, the embodiment of Fig. 8 may be viewed as an extreme version of the embodiment of Fig. 7 wherein the individual lateral plates positioned alongside the heat exchange conduit are not spaced apart, as seen in Fig. 7, but instead are positioned face-to-face with one another such that their conduit-side edges form the curved plates 620 of Fig. 8.

It will be apparent to those skilled in the art that other changes and modifications may be made in the above-described apparatus and methods for enhancing crossflow heat transfer without departing from the scope of the invention herein, and it is intended that all matter contained in the above description shall be interpreted in an illustrative and not a limiting sense.

CLAIMS

1. A baffle structure for preferentially contouring the flow path of a process fluid flowing cross-wise across and contacting a plurality of spaced-apart heat transfer surfaces, said structure comprising at least a paired set of fluid flow constrictors defining a substantially cross-wise flow path associated with a heat transfer surface, said fluid flow constrictors being located respectively in at least partial upstream and downstream alignment with each other and with the associated heat transfer surface, or along opposite sides of the associated heat transfer surface, or both, so as to contour the flow path of said process fluid around the heat transfer surface to realize improved thermal contact with the surface.
2. A baffle structure according to claim 1 wherein the fluid flow constrictors associated with a heat transfer surface comprise multiple pairs of fluid flow constriction apertures in baffles spaced respectively upstream and downstream from a heat transfer surface.
3. A baffle structure according to claim 2 wherein said heat transfer surfaces comprise the exterior surfaces of an array of heat exchange conduits oriented to have parallel axes, and the multiple pairs of apertures associated with a heat exchange conduit are aligned in columns parallel to the axis of the associated conduit.
4. A baffle structure according to claim 2 wherein said heat transfer surfaces comprise the exterior surfaces of at least one generally circular array of heat exchange

conduits oriented to have parallel axes, and said baffles spaced upstream and downstream from the heat exchange conduits comprise concentric apertured cylindrical plates having axially disposed columns of apertures, each array of heat exchange conduits being disposed in the annular region between two of said apertured cylindrical plates.

5. A baffle structure according to claim 4 wherein each pair of fluid flow constriction apertures comprise holes in radial alignment with the axis of said concentric cylindrical plates.

6. A baffle structure according to claim 4 wherein each pair of fluid flow constriction apertures comprise elongated slots, each slot having a long axis generally parallel to the axis of the associated heat exchange conduit.

7. A baffle structure according to claim 6 wherein pairs of elongated slots are in radial alignment.

8. A baffle structure according to claim 6 wherein a heat exchange conduit is associated with two pairs of elongated slots, each slot pair being offset from radial alignment with the axis of said concentric cylindrical plates.

9. A baffle structure according to claim 8 wherein the two upstream and two downstream elongated slots associated with a heat exchange conduit are axially offset from one another.

10. A baffle structure according to claim 1 wherein said heat transfer surfaces comprise the exterior surfaces of at least one generally circular array of heat exchange conduits oriented to have parallel axes, at least some of which are at least partially surrounded by substantially concentric apertured sleeves having upstream and downstream aperture pairs in columns parallel to the axis of the associated conduit, further wherein each concentric shell is secured by a plate member to adjacent concentric shells in the circular array to form a larger cylindrical structure.
11. A baffle structure according to claim 10 wherein the aperture pairs comprise elongated slots, each slot having a long axis generally parallel to the axis of the associated heat exchange conduit.
12. A baffle structure according to claim 11 wherein pairs of elongated slots are in radial alignment.
13. A baffle structure according to claim 11 wherein a heat exchange conduit is associated with two pairs of elongated slots, each slot pair being offset from radial alignment with the axis of the larger cylindrical structure.
14. A baffle structure according to claim 13 wherein the two upstream and two downstream elongated slots associated with a heat exchange conduit are axially offset from one another.

15. A baffle structure according to claim 10 wherein said heat transfer surfaces comprise the exterior surfaces of at least two generally concentric arrays of heat exchange conduits.
16. A baffle structure according to claim 15 wherein the aperture pairs comprise elongated slots in radial alignment, each slot having a long axis generally parallel to the axis of the associated heat exchange conduit.
17. A baffle structure according to claim 2 wherein said heat transfer surfaces comprise the exterior surfaces of a substantially rectangular array comprising at least two aligned rows of heat exchange conduits oriented to have parallel axes, and wherein said baffles comprise apertured plate members located upstream of the first row of heat exchange conduits, downstream of the last row of heat exchange conduits, and between each row of heat exchange conduits.
18. A baffle structure according to claim 17 wherein said fluid flow constriction apertures comprise columns of apertures in said plate members, said columns of apertures being aligned with the respective axes of the associated heat exchange conduits.
19. A baffle structure according to claim 2 wherein said heat transfer surfaces comprise the exterior surfaces of a substantially rectangular array comprising at least three aligned rows of cylindrical heat exchange conduits oriented to have parallel axes, and wherein said baffles comprise either: (a) apertured plate members located upstream of the first row of heat exchange conduits, downstream of the last row of heat exchange

conduits, and between each row of heat exchange conduits; or (b) apertured sleeve members having upstream and downstream aperture pairs.

20. A baffle structure according to claim 2 wherein said heat transfer surfaces comprise the exterior surfaces of a substantially rectangular array comprising at least three rows of cylindrical heat exchange conduits, with alternate rows offset from adjacent upstream and downstream rows, the heat exchange conduits oriented to have parallel axes, and wherein said baffles comprise either: (a) apertured plate members located upstream of the first row of heat exchange conduits, downstream of the last row of heat exchange conduits, and between each row of heat exchange conduits; or (b) apertured sleeves having upstream and downstream aperture pairs.

21. A baffle structure according to claim 1 wherein the fluid flow constrictors associated with a heat transfer surface comprise substantially flat plate members positioned in pairs edgewise alongside two sides of a heat transfer surface in proximity to the surface, said plate members being oriented generally orthogonal to said flow path.

22. A baffle structure according to claim 1 wherein the fluid flow constrictors associated with a heat transfer surface comprise plate members positioned in pairs alongside two respective sides of the heat transfer surface in proximity to the surface, said plate members having a contour corresponding to the two respective sides of the heat transfer surface so as to create channels having upstream and downstream openings along the two sides of the heat transfer surface, said plate members being joined to other plate members associated with adjacent heat transfer surfaces.

23. A baffle structure according to claim 1 further wherein a heat transfer surface comprises heat-transfer enhancing structures.
24. A baffle structure according to claim 23 wherein said heat-transfer enhancing structures comprise fin elements.
25. A method for enhancing heat transfer to or from a fluid flowing cross-wise in contact with the outer surfaces of a plurality of axially-oriented heat exchange conduits comprising the step of preferentially contouring fluid flow across the outer surfaces by flowing the fluid in a direction generally orthogonal to the axis of a heat exchange conduit, through at least a paired set of fluid flow constrictors associated with said heat exchange conduit in at least partial upstream and downstream alignment with each other and with the associated heat exchange conduit, or along two sides of the associated heat exchange conduit, or both.
26. A method according to claim 25 wherein said fluid is flowed through at least an aperture in a baffle upstream of a heat exchange conduit, contacted with the associated heat exchange conduit, and thereafter flowed through at least an aperture in a baffle downstream of the heat exchange conduit.
27. A method according to claim 26 wherein the apertures in the baffles comprise elongated slots.

28. A method according to claim 26 wherein said fluid is flowed through two apertures, each offset from the direction of fluid flow, in a baffle upstream of a heat exchange conduit, contacted with the associated heat exchange conduit, and thereafter flowed through two apertures, each offset from the direction of fluid flow, in a baffle downstream of the heat exchange conduit.

29. A method according to claim 25 wherein said fluid is flowed through an array comprising at least one upstream and one downstream row of heat exchange conduits in which a heat exchange conduit is associated with at least a paired set of fluid flow constrictors.

30. A method according to claim 29 comprising three or more rows of heat exchange conduits wherein said fluid flow constrictors comprise either: (a) apertured plate members located upstream of the first row of heat exchange conduits, downstream of the last row of heat exchange conduits, and between each row of heat exchange conduits; or (b) apertured sleeves having upstream and downstream aperture pairs.

31. A method according to claim 30 wherein said rows of heat exchange conduits are aligned to create substantially linear channels through the array.

32. A method according to claim 31 wherein the fluid is flowed through the array in a direction orthogonal to the rows of heat exchange conduits.

33. A method according to claim 31 wherein the fluid is flowed through the array in a direction diagonal to the planes of the rows of heat exchange conduits.

34. A method according to claim 30 wherein alternate rows of heat exchange conduits are offset relative to one another.

35. A method according to claim 34 wherein fluid is flowed through the array in a direction orthogonal to the planes of the rows of heat exchange conduits.

36. A method according to claim 34 wherein fluid is flowed through the array in a direction diagonal to the planes of the rows of heat exchange conduits.

37. A method according to claim 25 wherein said fluid is flowed through channels along two respective sides of a heat exchange conduit, said channels being defined by at least a pair of substantially flat plate members positioned edgewise alongside the two respective sides of the heat exchange conduit, in proximity to the outer surface of the heat exchange conduit, the plate members being oriented generally orthogonal to the direction of fluid flow.

38. A method according to claim 25 wherein said fluid is flowed through channels along two respective sides of a heat exchange conduit, said channels being defined by a pair of plate members positioned alongside the two respective sides of the heat exchange conduit in proximity to the outer surface of the conduit, said plate members having a

contour corresponding to the two respective sides of the heat exchange conduit and being joined to other plate members associated with adjacent heat exchange conduits.

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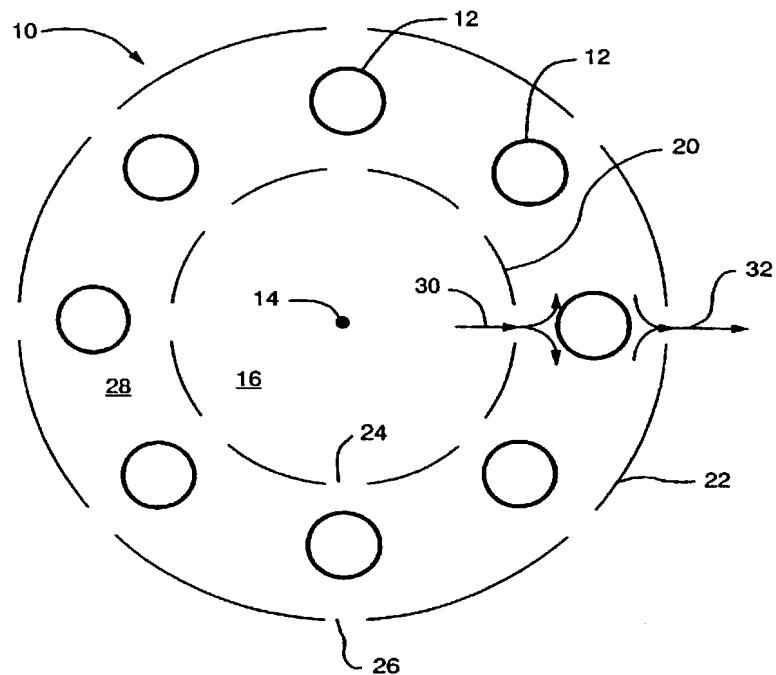
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(54) Title: ENHANCED CROSSFLOW HEAT TRANSFER



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(57) Abstract: Baffles (20, 22) arranged alongside a plurality of conduits (12).

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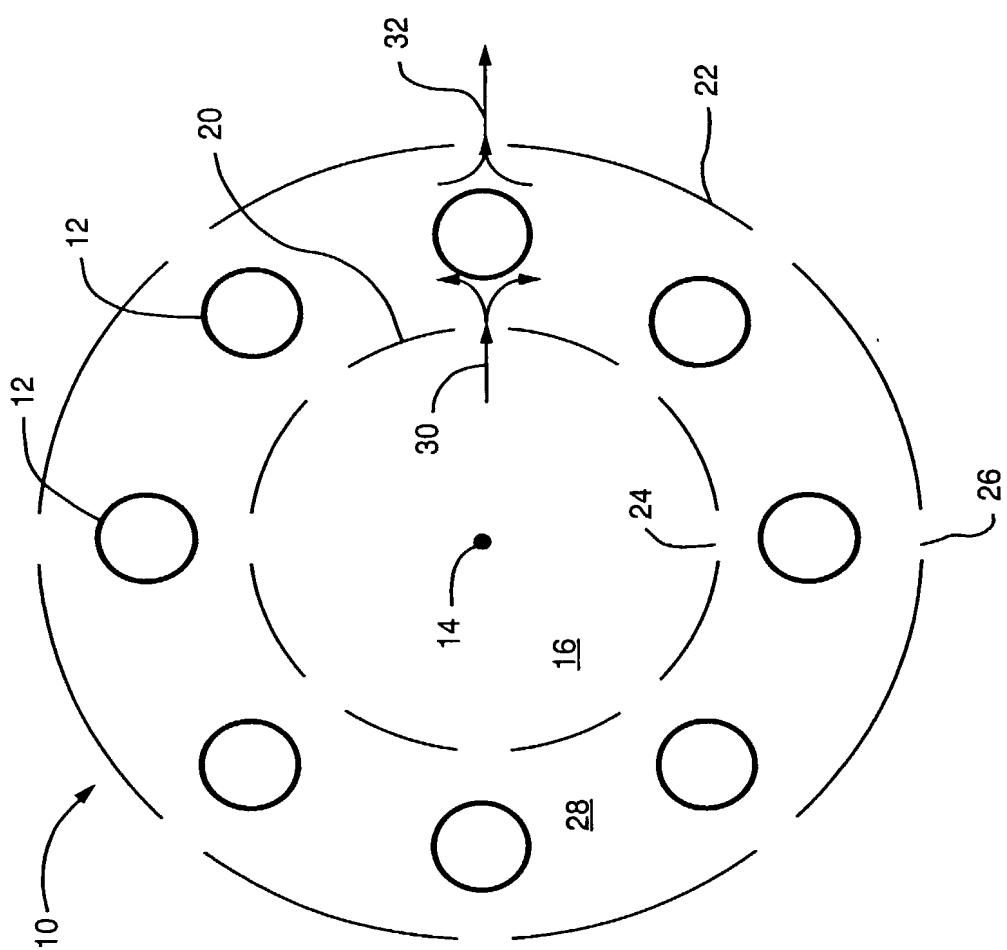


FIG. 1

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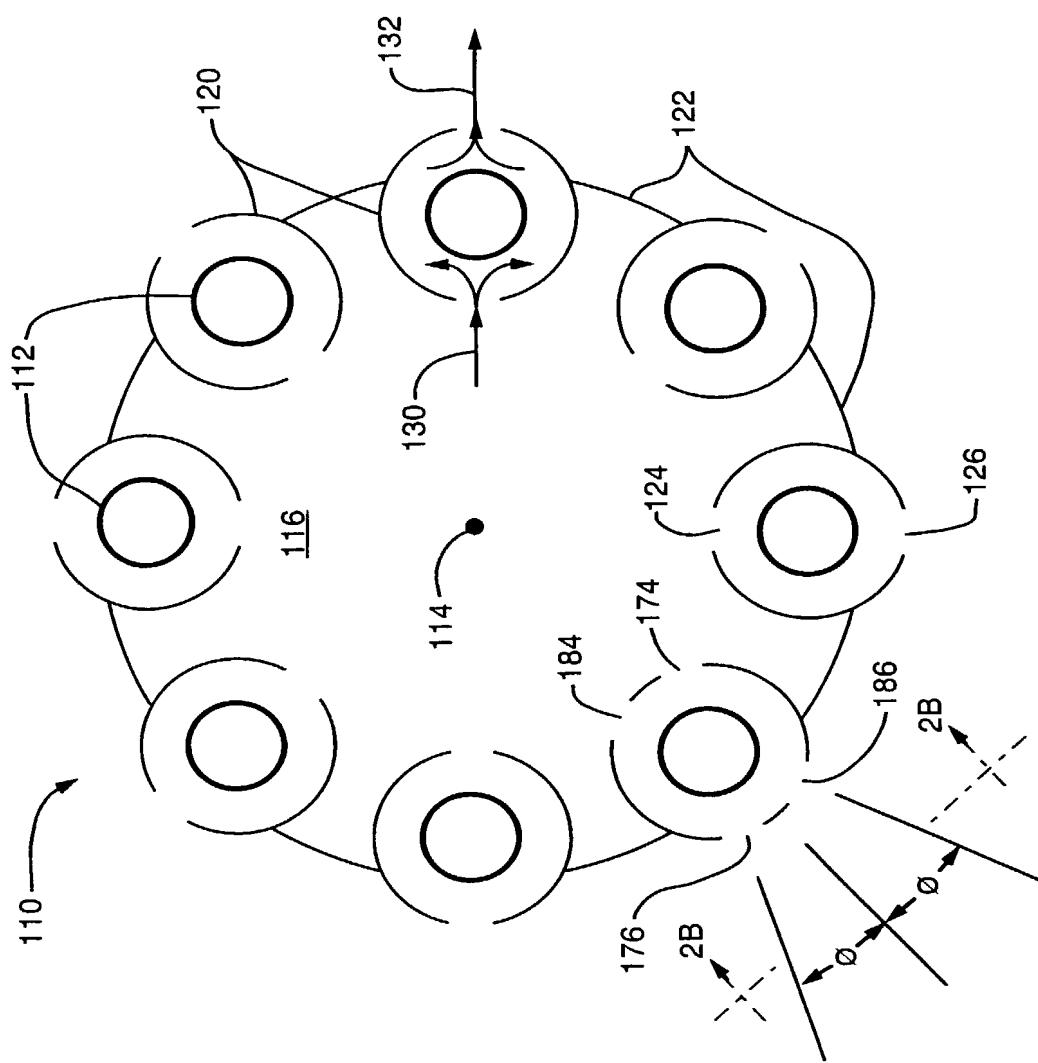


FIG. 2A

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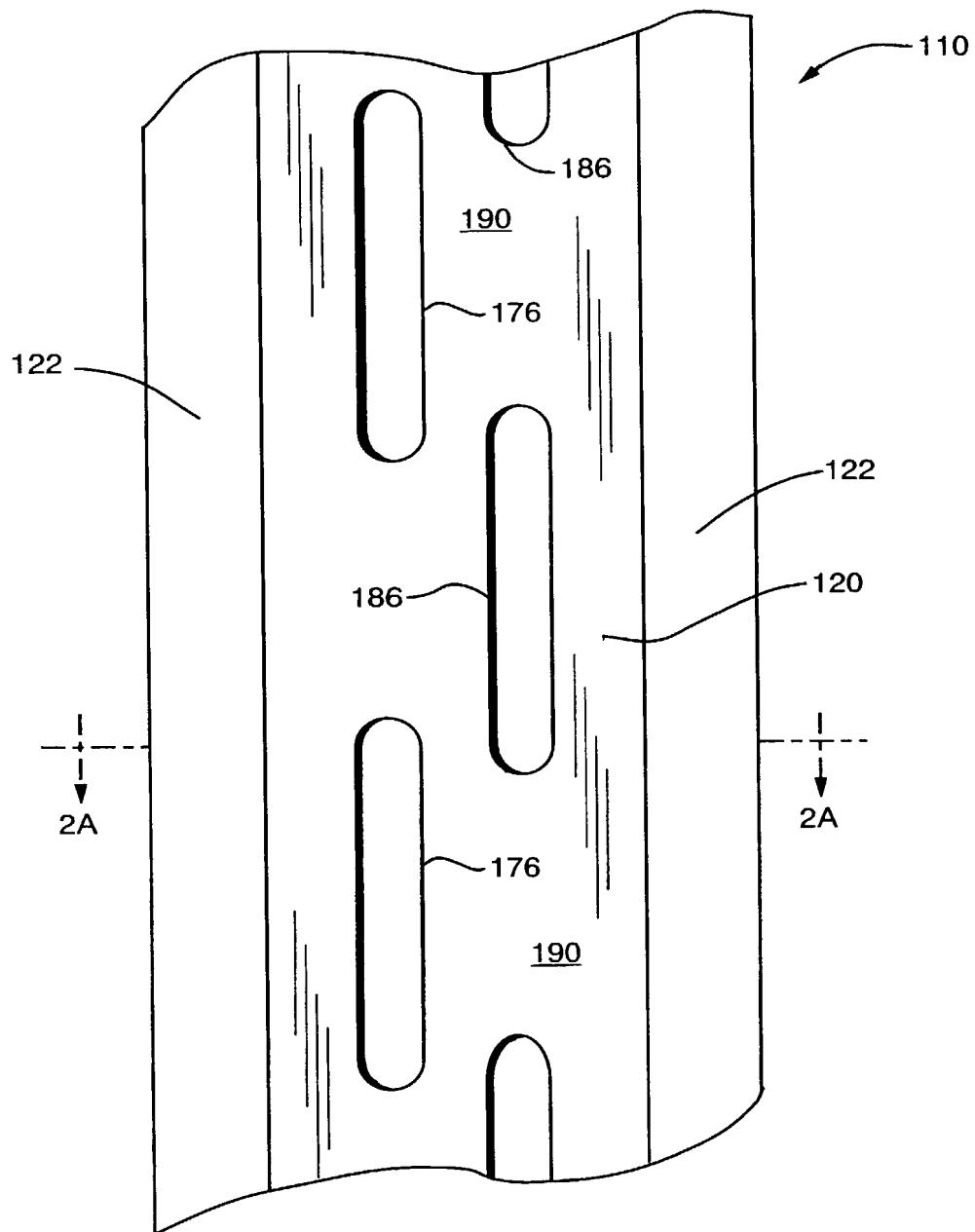
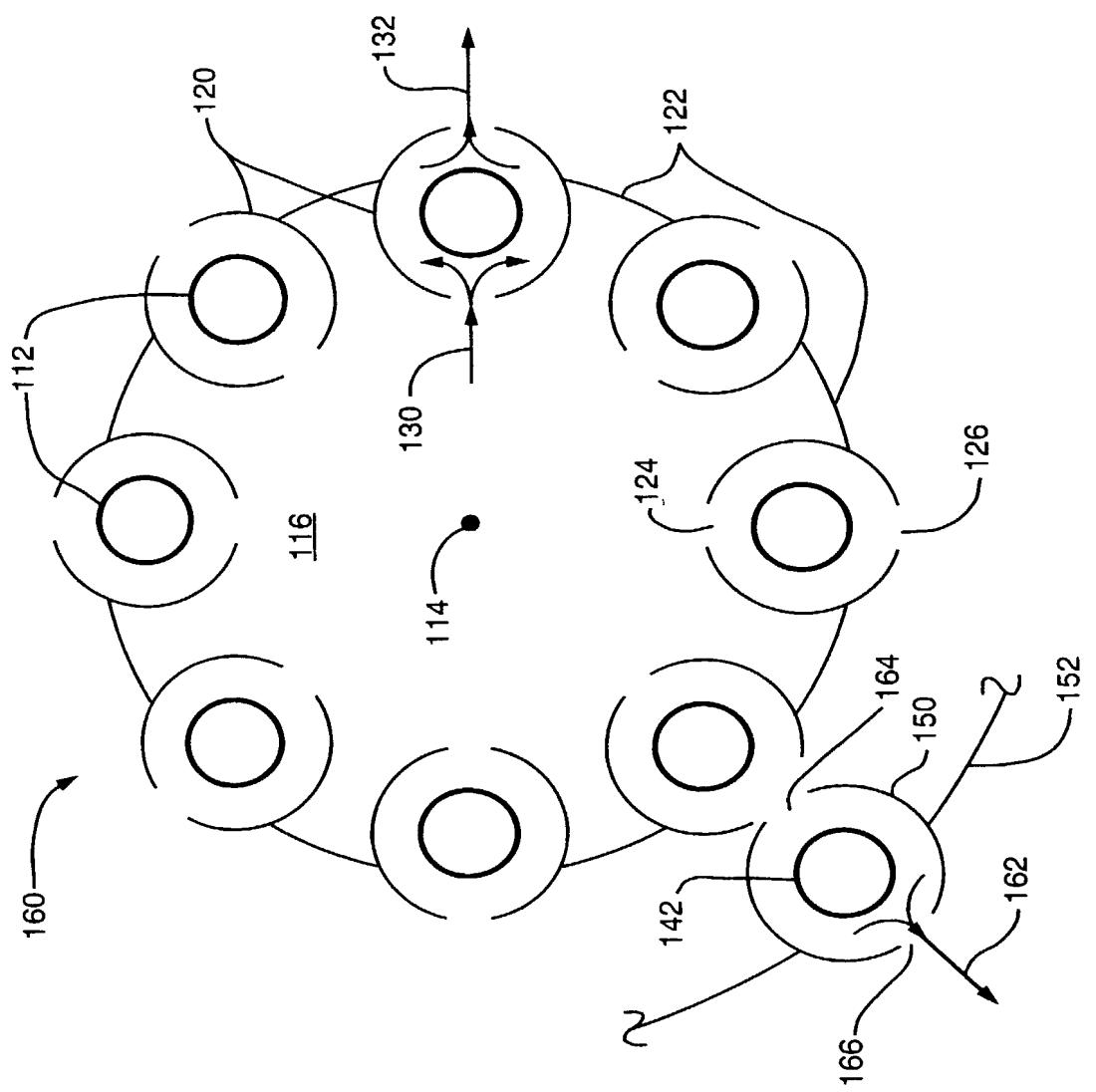


FIG. 2B



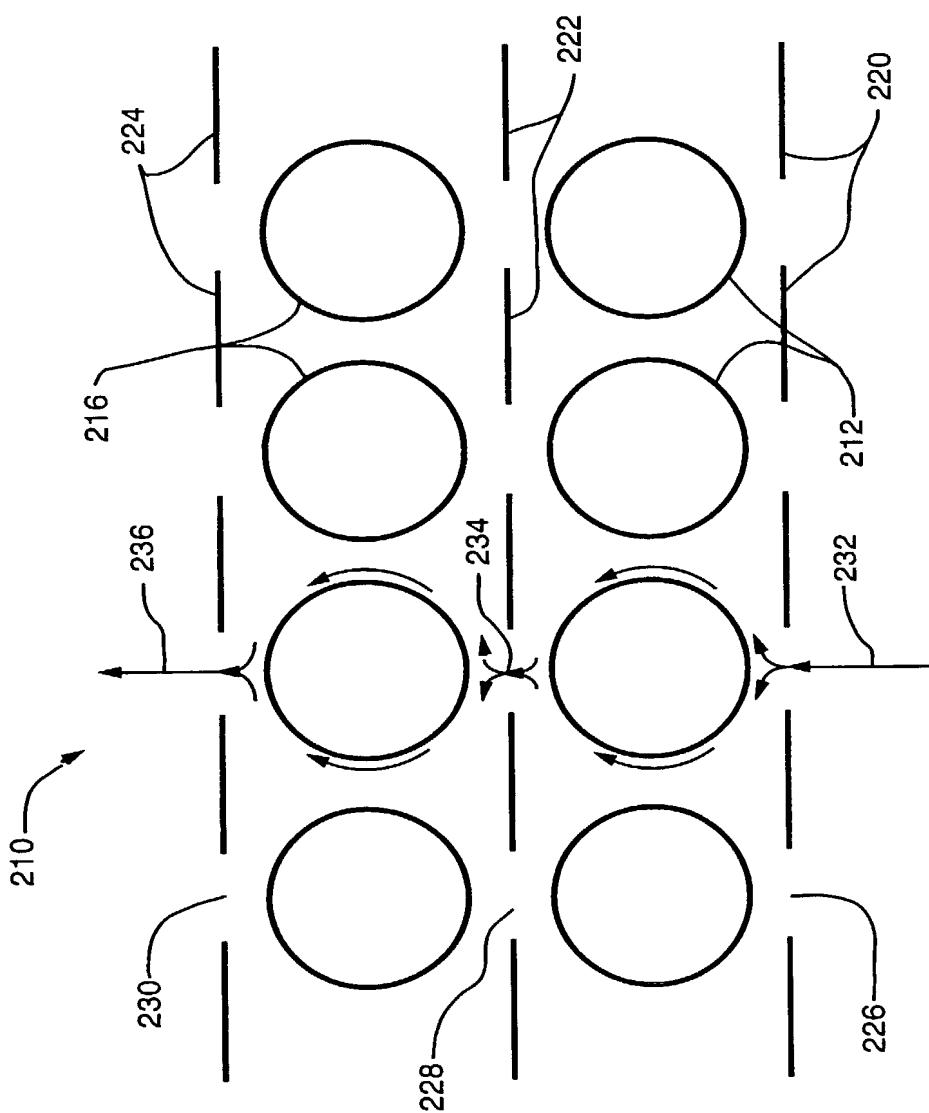


FIG. 4

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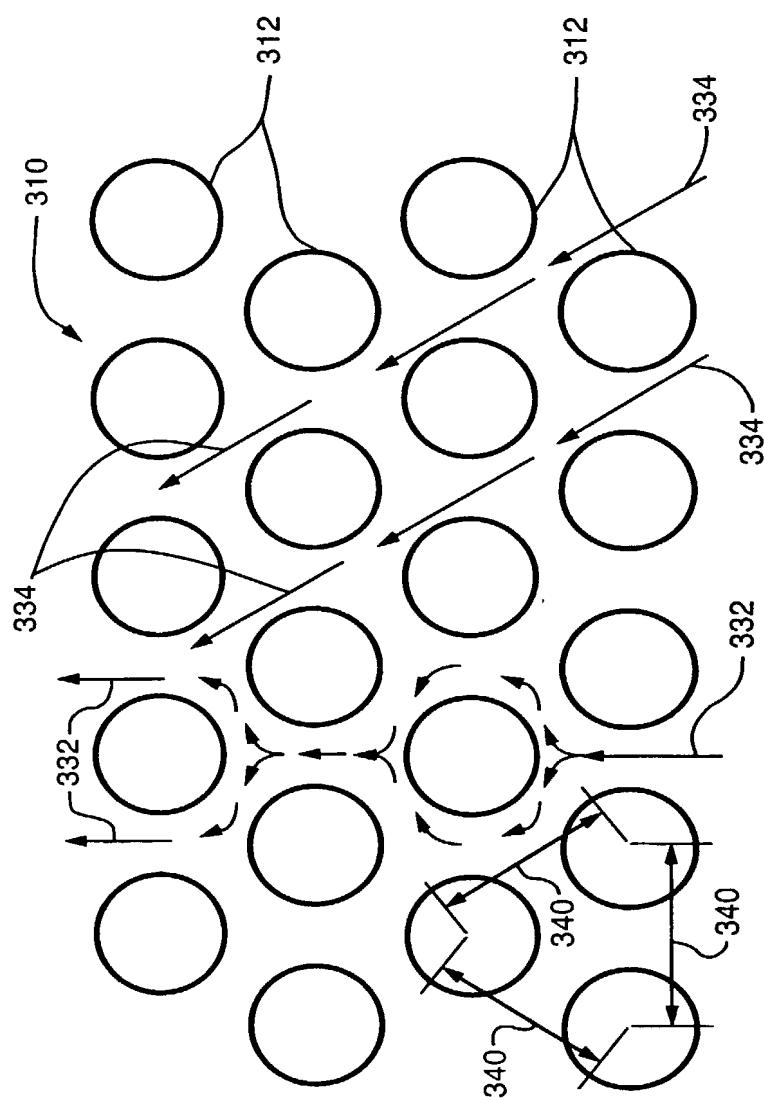


FIG. 5

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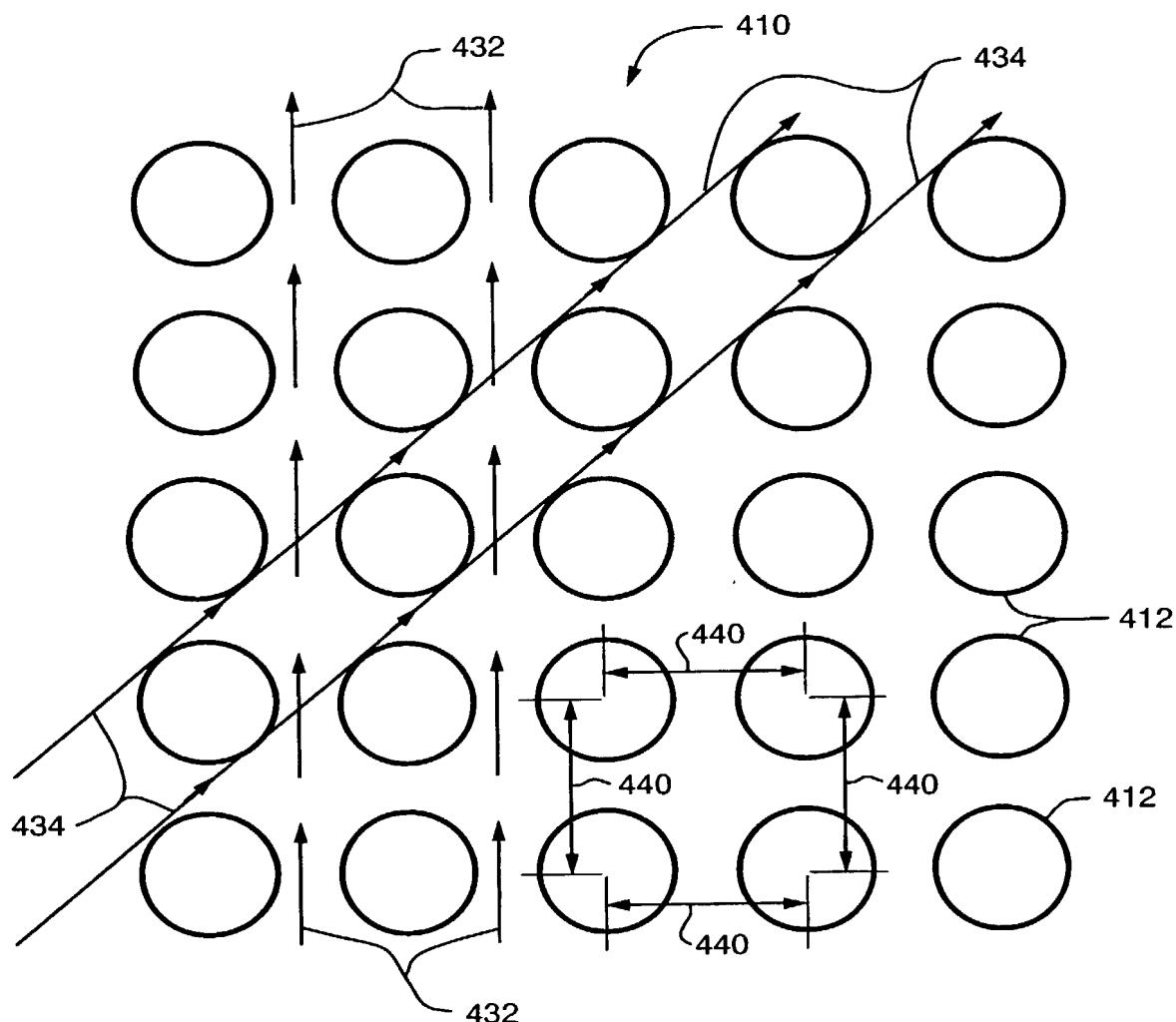


FIG. 6

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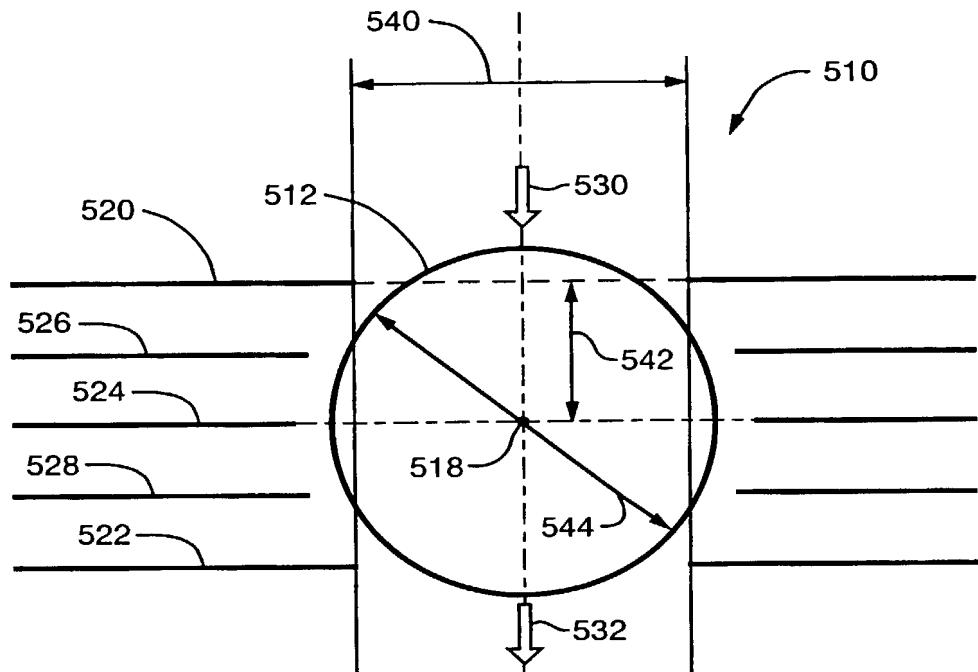


FIG. 7

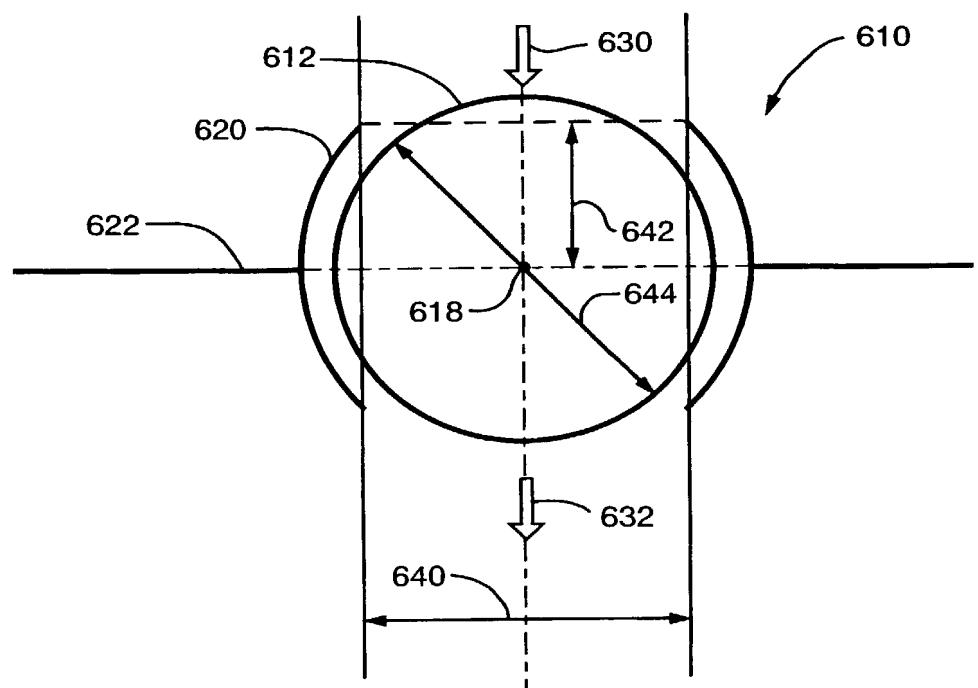


FIG. 8

COMBINED DECLARATION FOR PATENT APPLICATION AND POWER OF ATTORNEY  
(Includes Reference to PCT International Applications)ATTORNEY'S DOCKET NUMBER  
BGR-017PCT/US

As a below named inventor, I hereby declare that:

My residence, post office address and citizenship are as stated below next to my name.

I believe I am the original, first and sole inventor (if only one name is listed below) or an original, first and joint inventor (if plural names are listed below) of the subject matter which is claimed and for which a patent is sought on the invention entitled:

Enhanced Crossflow Heat Transfer

the specification of which (check only one item below):

 is attached hereto. was filed as United States applicationSerial No. 10/048,129on Jan. 14, 2002

and was amended

on \_\_\_\_\_ (if applicable).

 was filed as PCT international applicationNumber PCT/US00/40401on 18 July 2000 (18.07.2000)

and was amended under PCT Article 19

on \_\_\_\_\_ (if applicable).

I hereby state that I have reviewed and understand the contents of the above-identified specification, including the claims, as amended by any amendment referred to above.

I acknowledge the duty to disclose information which is material to the examination of this application in accordance with Title 37, Code of Federal Regulations, §1.56(a).

I hereby claim foreign priority benefits under Title 35, United States Code, §119 of any foreign application(s) for patent or inventor's certificate or of any PCT international application(s) designating at least one country other than the United States of America listed below and have also identified below any foreign application(s) for patent or inventor's certificate or any PCT international application(s) designating at least one country other than the United States of America filed by me on the same subject matter having a filing date before that of the application(s) of which priority is claimed:

## PRIOR FOREIGN/PCT APPLICATION(S) AND ANY PRIORITY CLAIMS UNDER 35 U.S.C. 119:

COUNTRY (if PCT, indicate "PCT")	APPLICATION NUMBER	DATE OF FILING (Inv. Inventor, year)	PRIORITY CLAIMED UNDER 35 USC 119
PCT	PCT/US00/40401	18 July 2000 (18.07.2000)	<input checked="" type="checkbox"/> yes <input type="checkbox"/> no
			<input type="checkbox"/> yes <input type="checkbox"/> no
			<input type="checkbox"/> yes <input type="checkbox"/> no
			<input type="checkbox"/> yes <input type="checkbox"/> no
			<input type="checkbox"/> yes <input type="checkbox"/> no

## Combined Declaration For Patent Application and Power of Attorney (Continued)

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I hereby claim the benefit under Title 35, United States Code, §120 of any United States application(s) or PCT international application(s) designating the United States of America that is/are listed below and, insofar as the subject matter of each of the claims of this application is not disclosed in that/those prior application(s) in the manner provided by the first paragraph of Title 35, United States Code, §112, I acknowledge the duty to disclose material information as defined in Title 37, Code of Federal Regulations, §1.56(a) which occurred between the filing date of the prior application(s) and the national or PCT international filing date of this application.

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PCT/US00/40401	18 July 2000 (18.07.2000)	X

POWER OF ATTORNEY: As named inventor, I hereby appoint the following attorney(s) and/or agent(s) to prosecute this application and transact all business in the Patent and Trademark Office connected therewith. (List name and registration number)

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DATE ✓ 2/26/02	DATE ✓ 01/08/02	DATE

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